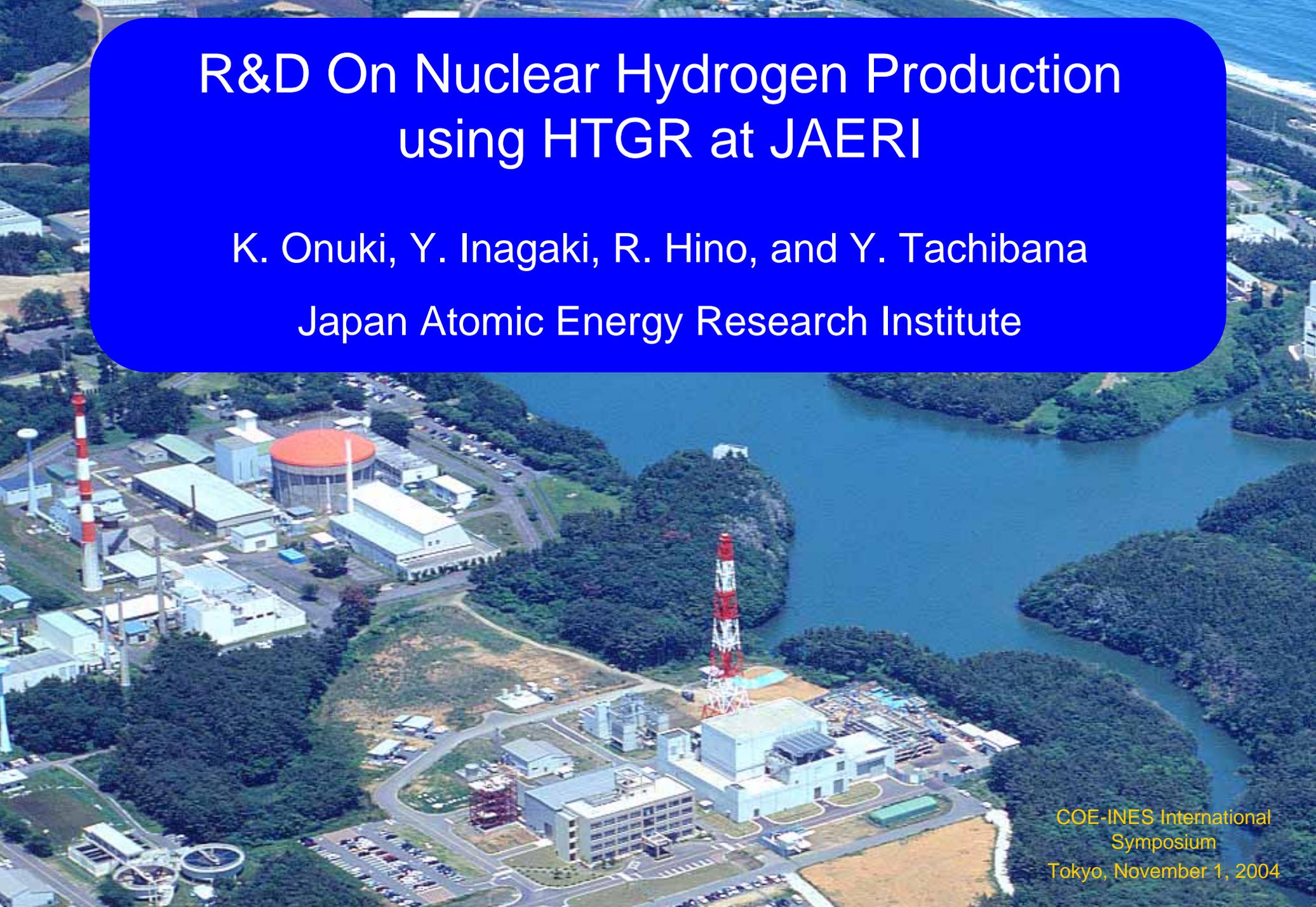


# R&D On Nuclear Hydrogen Production using HTGR at JAERI

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# Toward the Hydrogen Energy Society

Current Society depends on fossil energy

- Exhaustion of fossil energy
- Effects on global environment; acid rain, global warming, etc.

## Activities on Hydrogen in Japan

“Basic Plan for Energy Supply and Demand”  
based on “Basic Law on Energy Policy Making”  
(Decided upon by the Cabinet on 6 October, 2003)

Effort for Hydrogen Energy Utilization (Chapter 2, section 6.3)

- Hydrogen is a clean energy carrier without CO<sub>2</sub> emission.
- Commercialization of hydrogen production system using **nuclear**, solar and biomass, not fossil fuels, is desired.

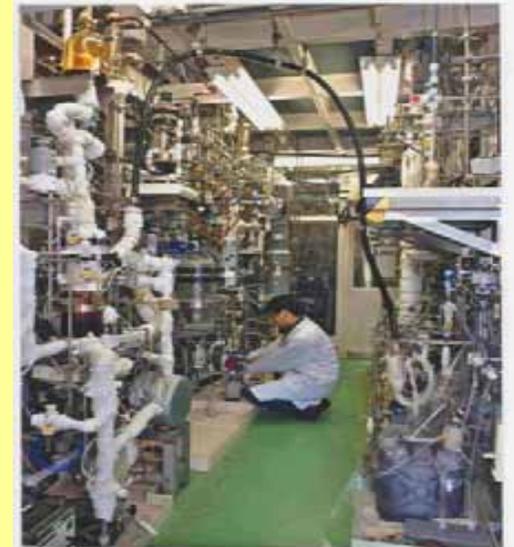
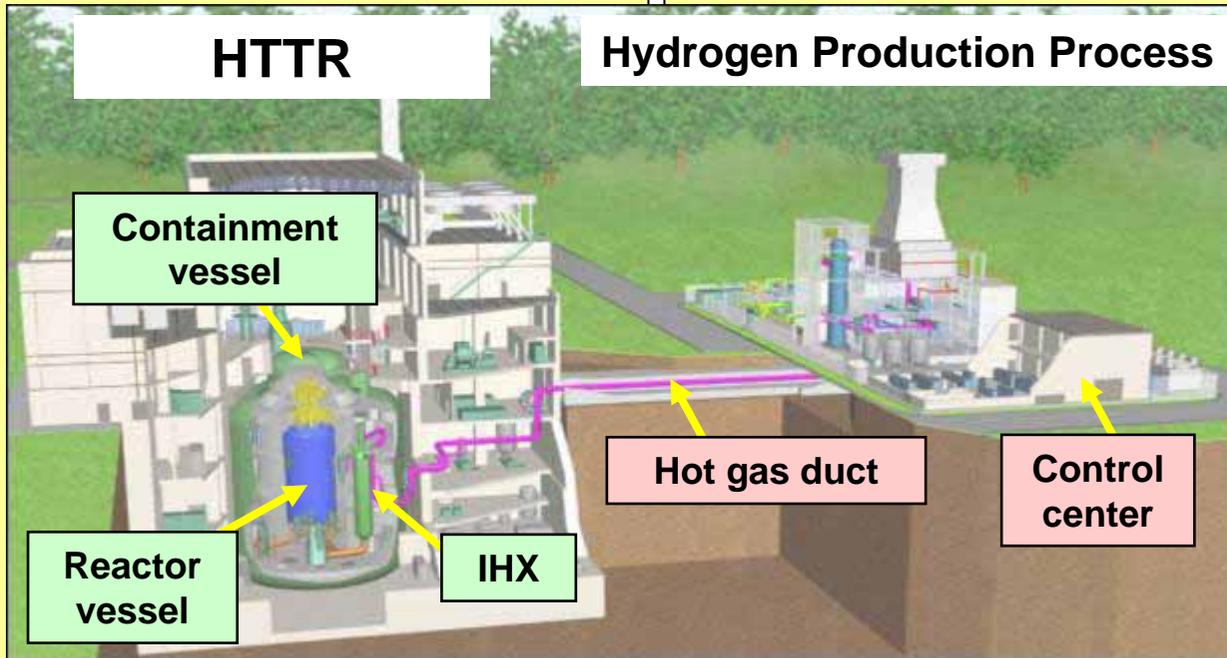
# Overview of R&D at JAERI

**Objective:** Establishment of HTGR technology  
Establishment of heat utilization technology

Reactor  
Technology

System Integration  
Technology

Hydrogen Production  
Technology



Bench-scale apparatus  
of IS Process



# System Integration Technology

## Objective

- Development of technology for safe and economical connection between reactor and hydrogen production facility

## R&D Items

### ➤ Safety technology against explosion

- Design for protection and mitigation against combustible gas release: underway
- Estimation of damage on nuclear plant by blast waves from explosion: underway

### ➤ Safety technology against radioactive materials release

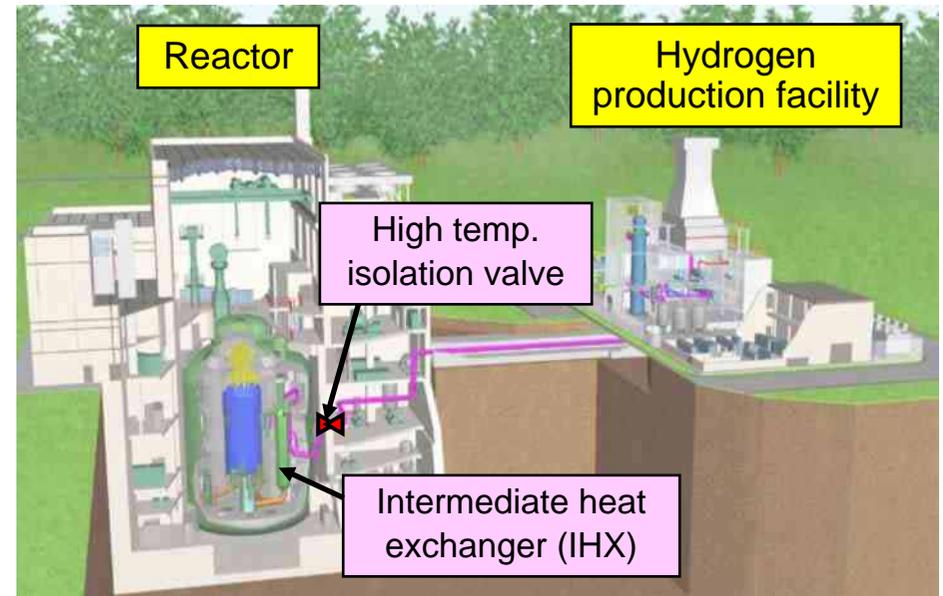
- Development of high temp. isolation valve: underway
- Estimation of tritium permeation passing through IHX: finished

### ➤ Control technology

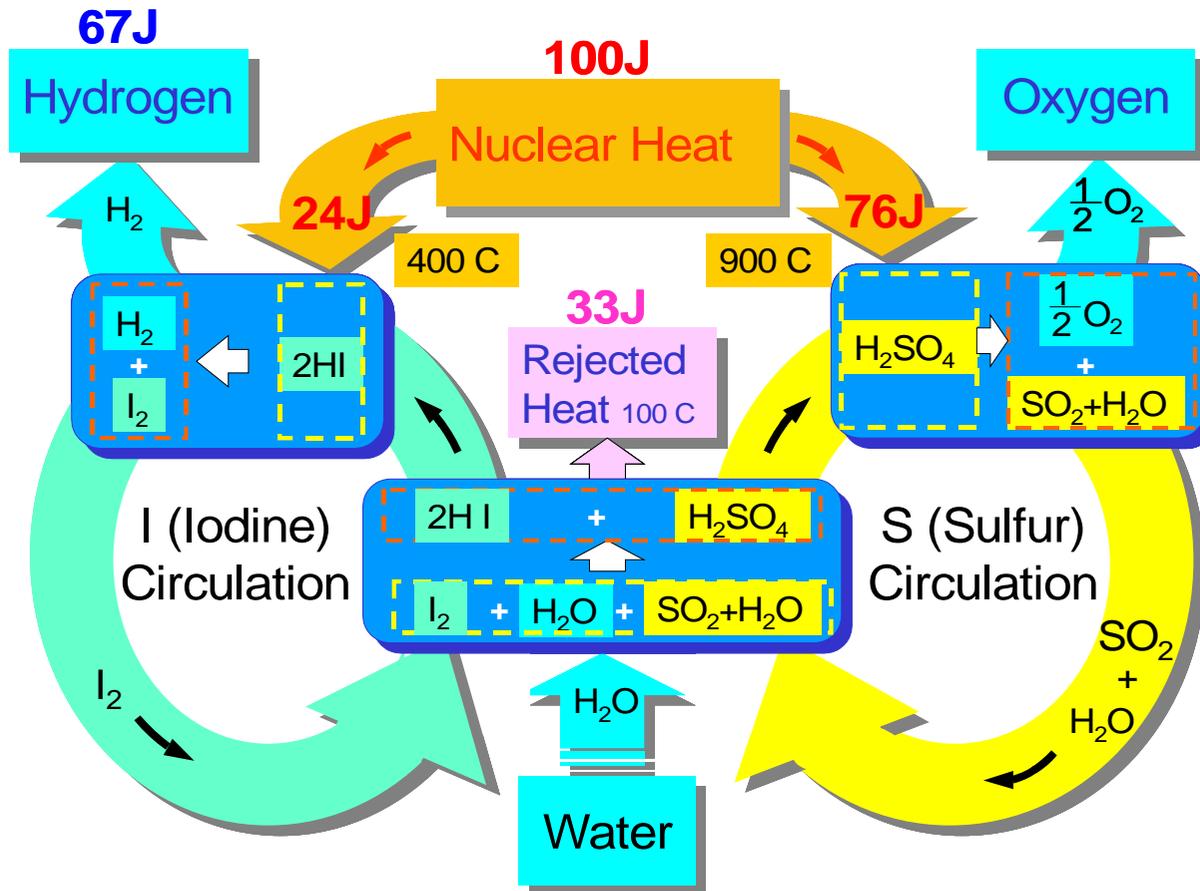
- Prevention of thermal disturbance from hydrogen production facility to reactor by steam generator : finished

### ➤ Plant simulation code

- Verification by simulation test: underway



# Hydrogen Production Technology



## IS Process

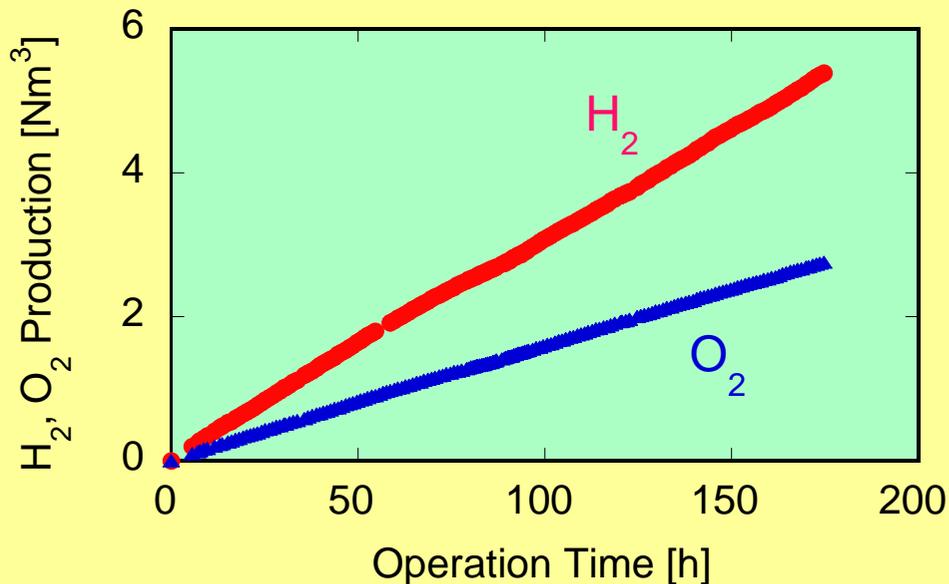
- **Hydrogen from water and nuclear heat (CO<sub>2</sub> free)**
- **Thermochemical cycle**
- **Iodine- and Sulfur-compounds are used as recycling materials**

# R&D on IS Process

## Completion of Hydrogen Production (June 2004)

Continuous hydrogen production was successfully achieved at the hydrogen production rate of 32 NL/h for 1 week.

[This study is entrusted from MEXT of Japan.]



Commercialization

HTTR Test (10MW, ~ 1000m<sup>3</sup>/h)

Pilot Test (0.4MW, ~ 30m<sup>3</sup>/h)

*He heating, Industrial materials,  
High pressure*

**Bench-scale Test**  
(1999-2004)

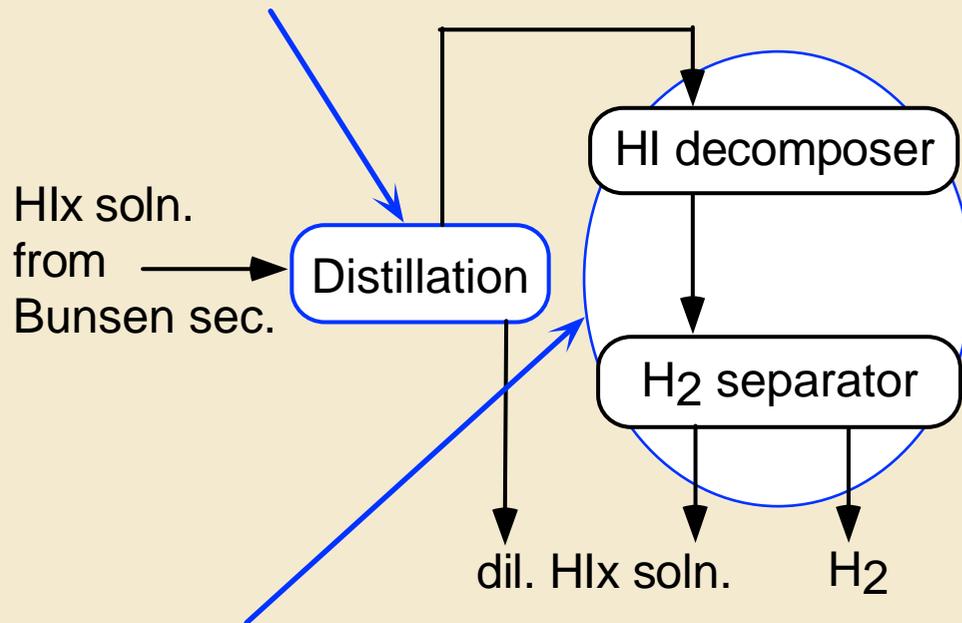
Lab-scale Test

*Verification of Theory (1997)*

# For efficient H<sub>2</sub> production,

## <Problems>

/ large thermal burden  
for the distillation of  
azeotropic hydriodic  
acid (HI/H<sub>2</sub>O: 1/5)



/ excess HI circulation due to  
low equilibrium conversion  
of HI (ca. 20%)

## <Approach>

- (1) Extractive distillation (GA)  
Destroy the azeotrope with H<sub>3</sub>PO<sub>4</sub>
- (2) Reactive distillation (RWTH Aachen)  
Shift the azeotropic composition  
at elevated pressure (e.g. 20bar).  
Carry out the decomposition in  
the distillation column.
- (3) Membrane separation (JAERI)  
Pre-concentrate the HIx soln. by  
electrodialysis.  
Enhance the one-pass conversion  
by membrane reactor.

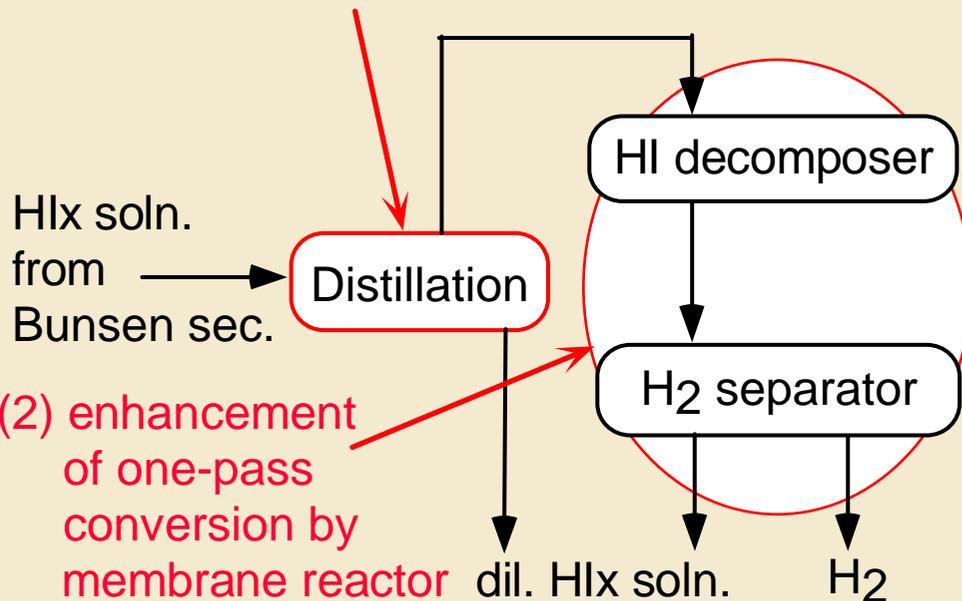
# JAERI's approach for efficient H<sub>2</sub> production

## <Problems>

- / large thermal burden for the distillation of azeotropic hydriodic acid (HI/H<sub>2</sub>O: 1/5)
- / excess HI circulation due to low equilibrium conversion of HI (ca. 20%)

## <Measures>

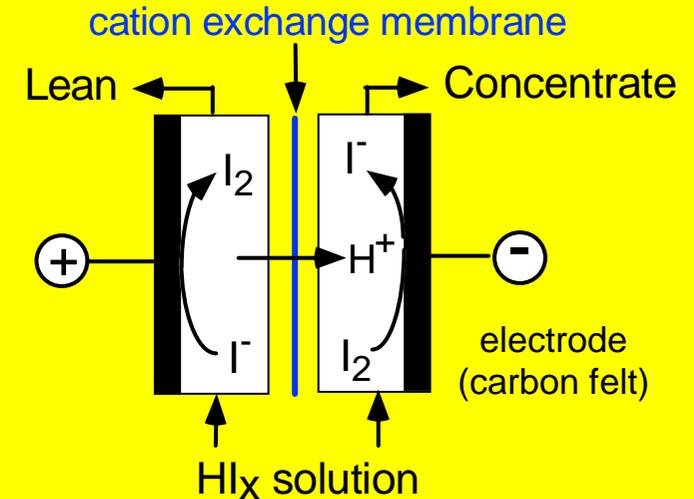
- (1) preconcentration to overazeotropic composition



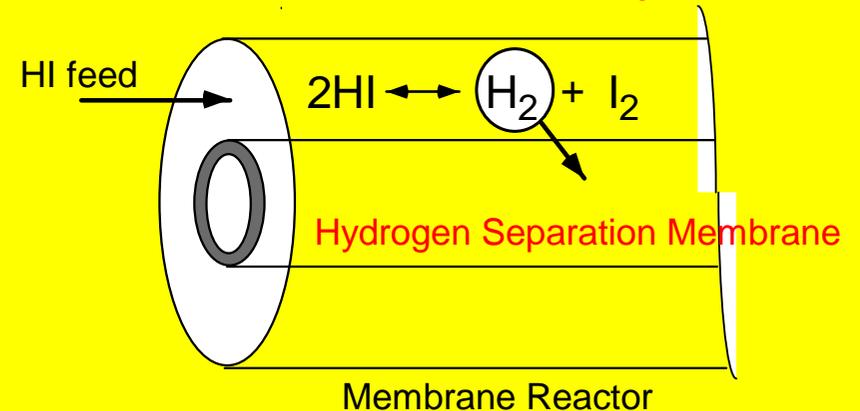
- (2) enhancement of one-pass conversion by membrane reactor

## Present study focuses on

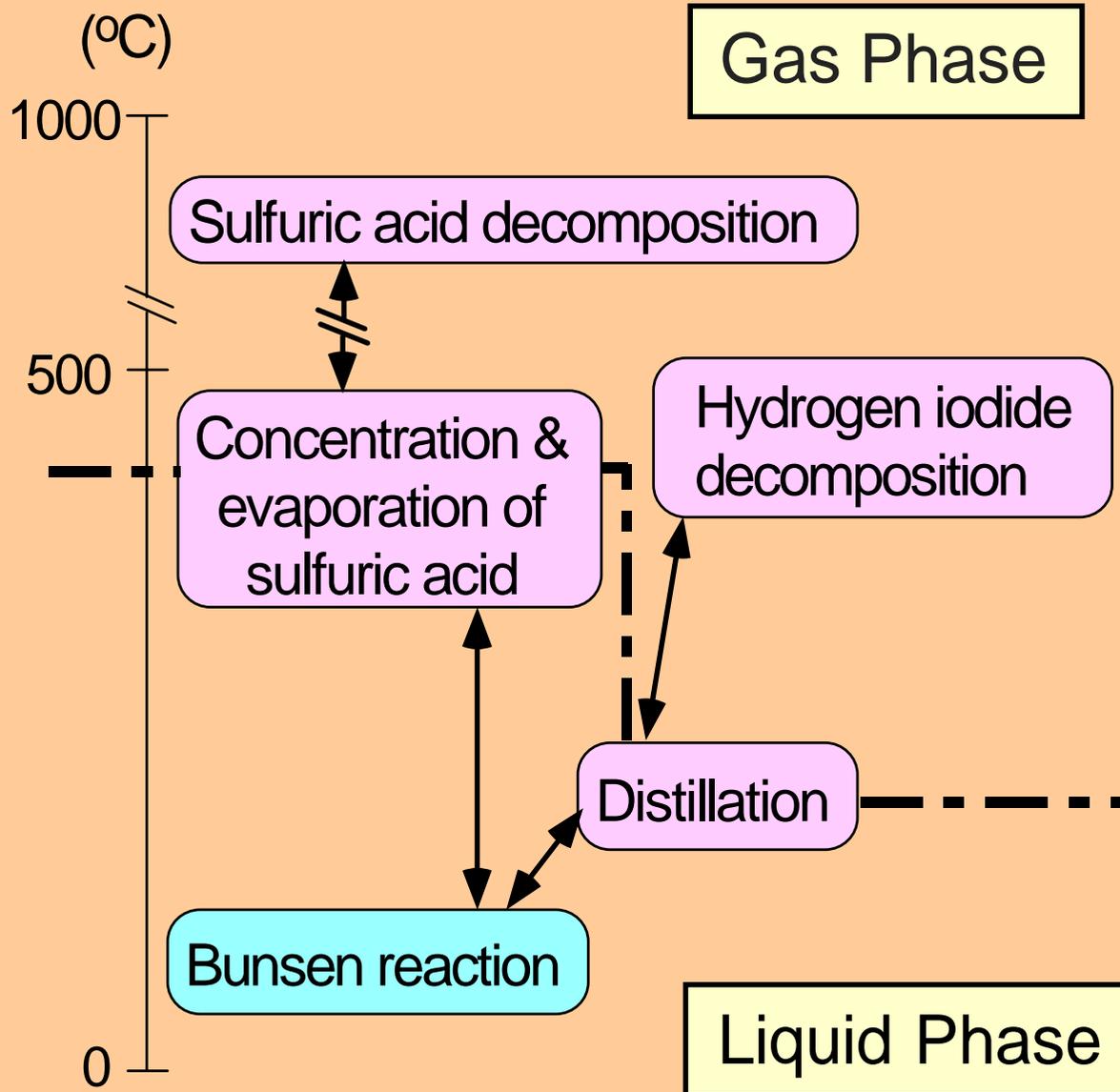
### (1) Electro-electrodialysis



### (2) Silica membrane for H<sub>2</sub> separation



# Corrosion Environments in IS Process



## *Sulfur Environments*

### Sulfuric Acid

50 - 96wt% Sulfuric acid  
90 - 500°C, 0.1 - 2 MPa  
minor component: Iodine

Gaseous  $\text{SO}_3$ ,  $\text{SO}_2$ ,  $\text{O}_2$   
500 - 900°C, 2 MPa

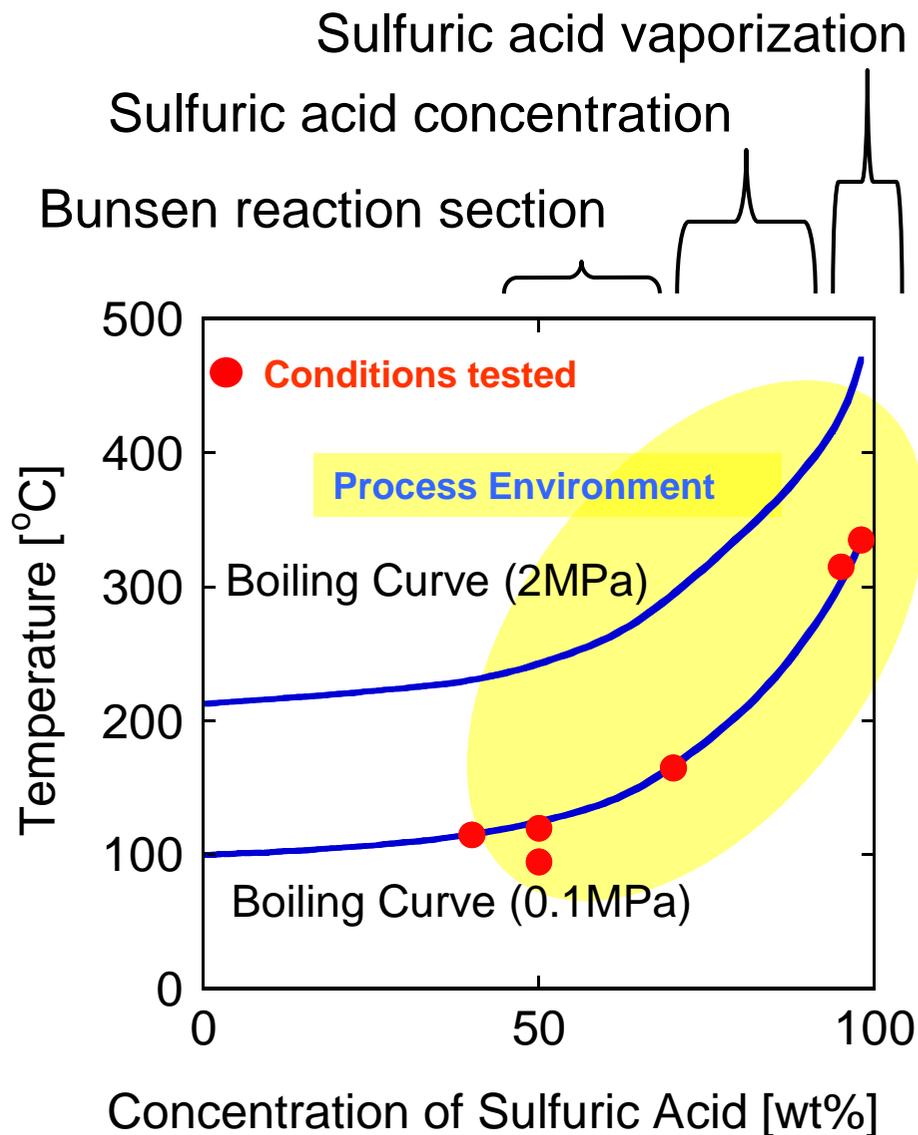
## *Iodine Environments*

### HIx Solution

HI-I<sub>2</sub>-H<sub>2</sub>O,  
90 - 200°C, 0.1 - 1 MPa

Gaseous HI, I<sub>2</sub>, H<sub>2</sub>, H<sub>2</sub>O  
200 - 500°C, 1 MPa

# Previous Corrosion Study in Sulfuric Acid at JAERI



Candidate materials for sulfuric acid service in IS process screened by the corrosion study carried out under atmospheric pressure condition

- For Bunsen reaction section  
Ta, Zr, SiC, Si<sub>3</sub>N<sub>4</sub>, SiO<sub>2</sub>, PFA
- For sulfuric acid concentration  
Ta, Zr, Fe-Si, SiSiC, SiC, Si<sub>3</sub>N<sub>4</sub>
- For sulfuric acid vaporization  
Fe-Si, SiSiC, SiC, Si<sub>3</sub>N<sub>4</sub>

# Corrosion Test under Pressurized Condition



**Autoclave**



Quartz ampoule with  
test piece and  
sulfuric acid

# Test Results in Sulfuric Acid

## Corrosion rates in 95wt% sulfuric acid\*1)

Material	Corrosion rate [g/m <sup>2</sup> h]	
	100hr test	1000hr test
SiC	- 0.10	- 0.002
Si-SiC	0.0	- 0.006
Si <sub>3</sub> N <sub>4</sub>	0.0	- 0.007
Fe-Si (as-prepared)	1.1	0.13
Fe-Si (annealed)*2)	- 0.12	0.065
SX (pre-oxidized) *3)	- 0.28	0.96 *4)

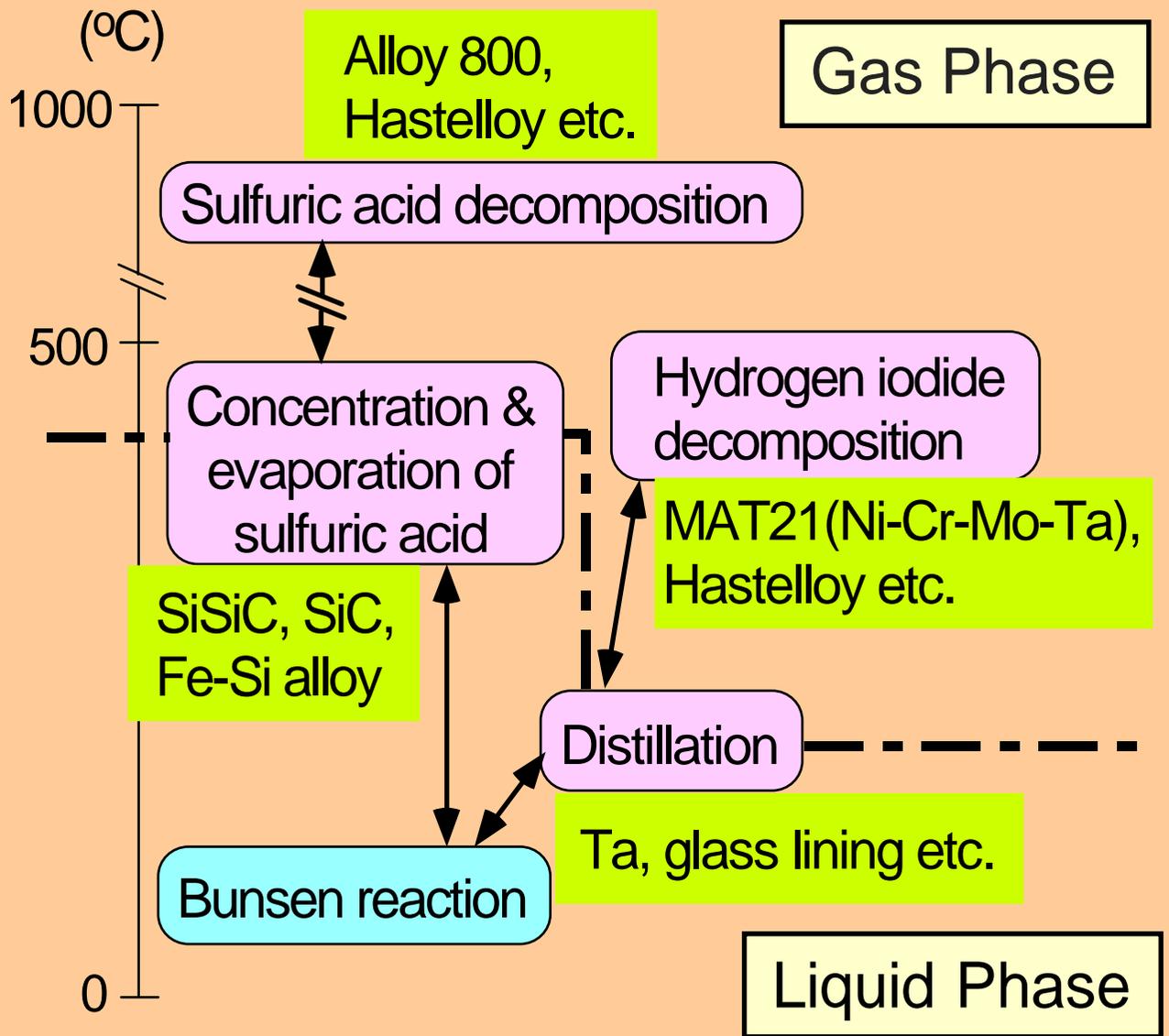
\*1) test conditions: 733K(460°C), 2MPa.

\*2) annealed at 1373K(1100°C) under vacuum for 100hr.

\*3) oxidized in air at 1073K(800°C) for 90hr.

\*4) test piece size: 4x4x20mm. ampoule broken after 800hr.

# Screening Results of Candidate Materials



Candidate materials has been screened by corrosion tests in the process condition.



R&D is required for the components used in the boiling sulfuric acid environments.

ex) hybridization of corrosion resistant material and pressure resistant material

# R&D Plan of IS Process in JAERI

Connection with HTTR



Pilot-Scale Test: 30m<sup>3</sup>/h



Advanced HI  
Processing  
(- FY2004)

Bench-Scale Test: 30NL/h  
(- FY2004)

Corrosion Resistant  
Materials  
(- FY2004)



Lab-Scale Test: 1NL/h